

Still Heating Technologies and Emulation of Direct Fired Character

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Briggs of Burton

Talk Outline

- Introduction
 - Still heating objectives
- Overview of Still Heating Technologies
 - Direct Fired
 - Internally Heated
 - Externally Heated
- Emulation of Direct Fired Character
 - Can the Pot Still Heating Method Influence Spirit Character?
 - Investigation using Novel Thermal Fluid (Oil) Heating Technology



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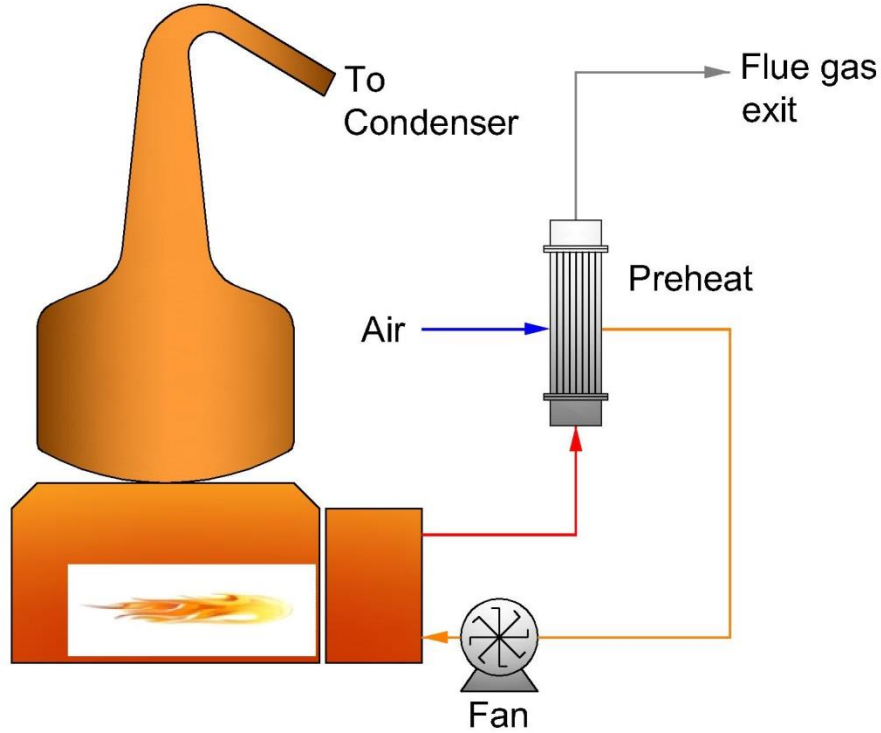
Still Heating Objectives

- Heat the Still to boiling
- Maintain a consistent evaporation rate from Batch start to the end
- Minimise fouling & Cleaning
- Controllable, reliable & safe.
- Minimise energy usage / Carbon footprint



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Direct Fired System



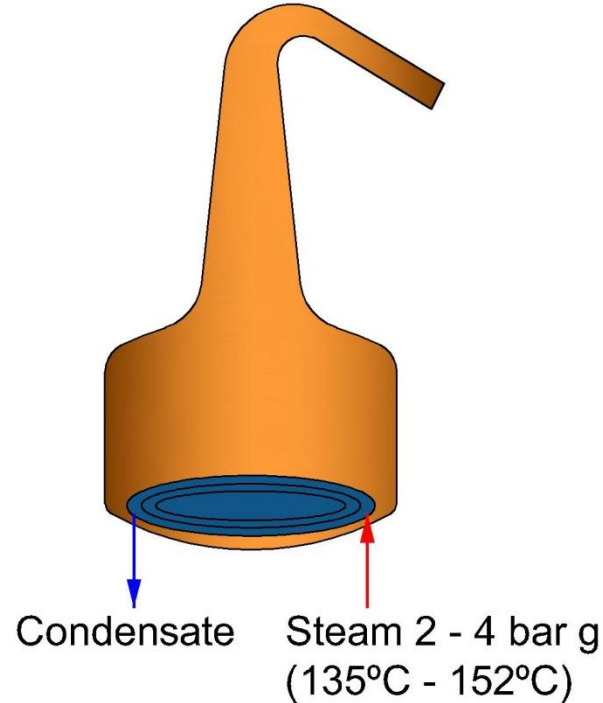
- Natural Gas Fired (typically) – flame temp 1200°C
- Flue Exit Temp 600°C
- Low Copper Surface Area > 200°C ($\sim 0.8 \text{ m}^2/\text{m}^3$)
- 9.2 kWh/litre pure alcohol (lpa)
- Preheated combustion air $\sim 15\%$ fuel saving
- Rummager – removal of fouling material produced continuously
- Refractory Lined 'Hot Box'



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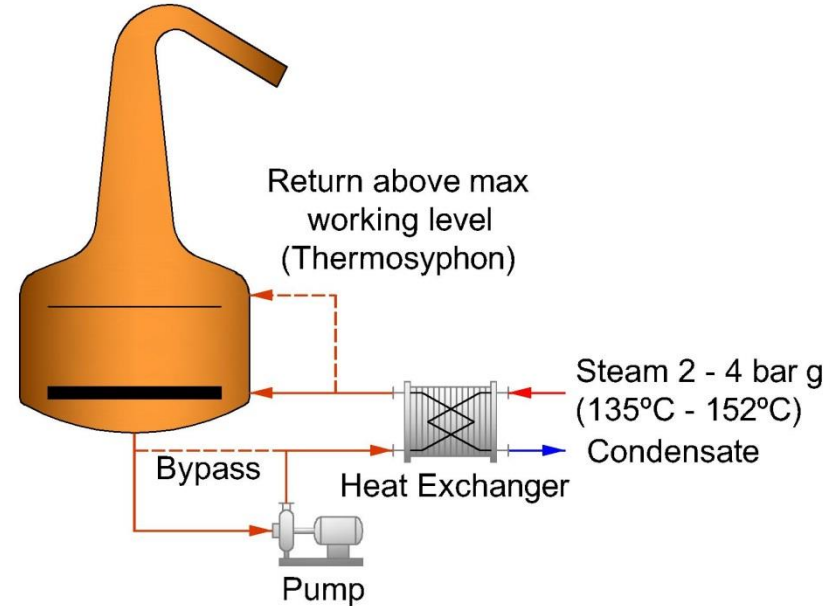
Internal Coil / Pans

- Steam Most Common
 - Potential for Thermal Fluid
- Stainless Steel Coil / Pan
- Energy
 - Low Heating Surface Area
 - 135 - 152°C (0.8 m²/m³)
 - Typically Isothermal Heating
 - 7.2 kWh / litre pure alcohol (lpa)
- Cleaning
 - Fouling Removed by Cleaning In Place (CIP)



External Heater (Plate or Shell & Tube)

- Wash does NOT boil in heat exchanger
- Min Height at End of Distillation is critical, Can dictate minimum Recirculation rate
- Check Net Positive Suction Head (NPSH)
- Heating Surface $135\text{-}152^{\circ}\text{C}$ ($1.0\text{ m}^2/\text{m}^3$)
- TVR/HTHP High Heating Surface Area $95\text{-}107^{\circ}\text{C}$ ($\sim 1.6\text{ m}^2/\text{m}^3$)

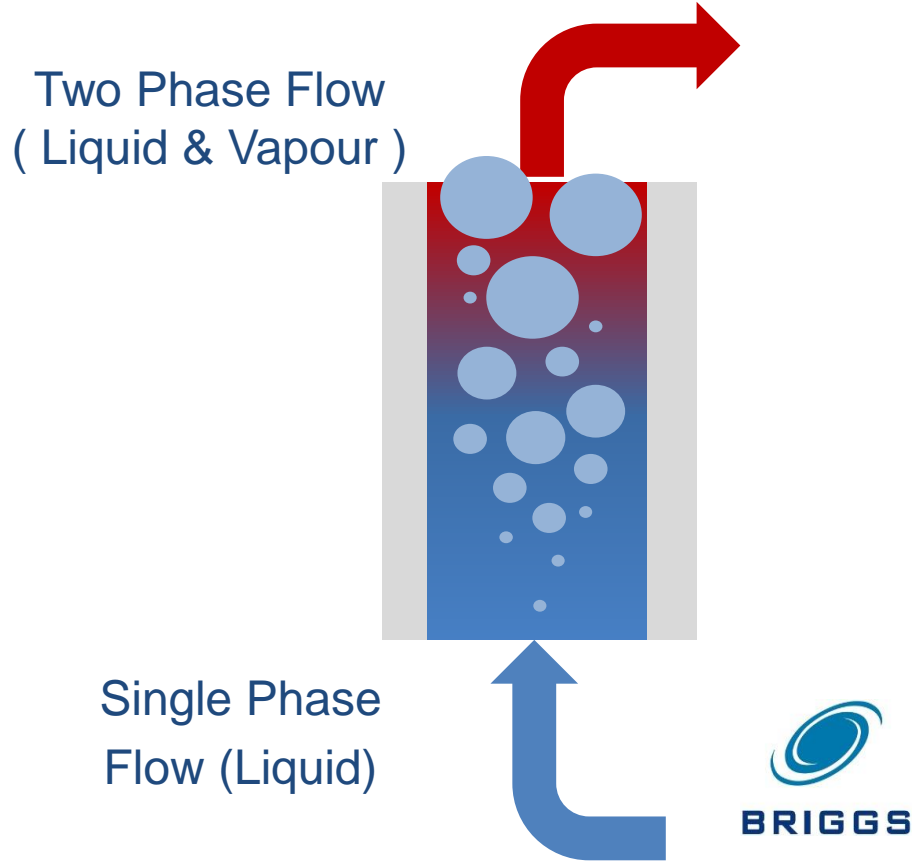


Pumped Recirculation - OPEX

- Recirculation pump operational cost often overlooked
 - $\sim 0.3 - 0.8 \text{ kWe/m}^3$
 - £2,400 – £5,900 cost p.a (per pump at 11p/kWh)
- Recirculation rate dependent on steam pressure and temp. raise per pass.
 - 6 - 15+ contents/hr.
- Thermosyphon during distillation could eliminate this cost
- Thermosyphon commonly used in brewing industry
- Vapour Bubbles Beneficial
 - Volatile Stripping
 - improved cogener recovery?

Thermosyphon Recirculation

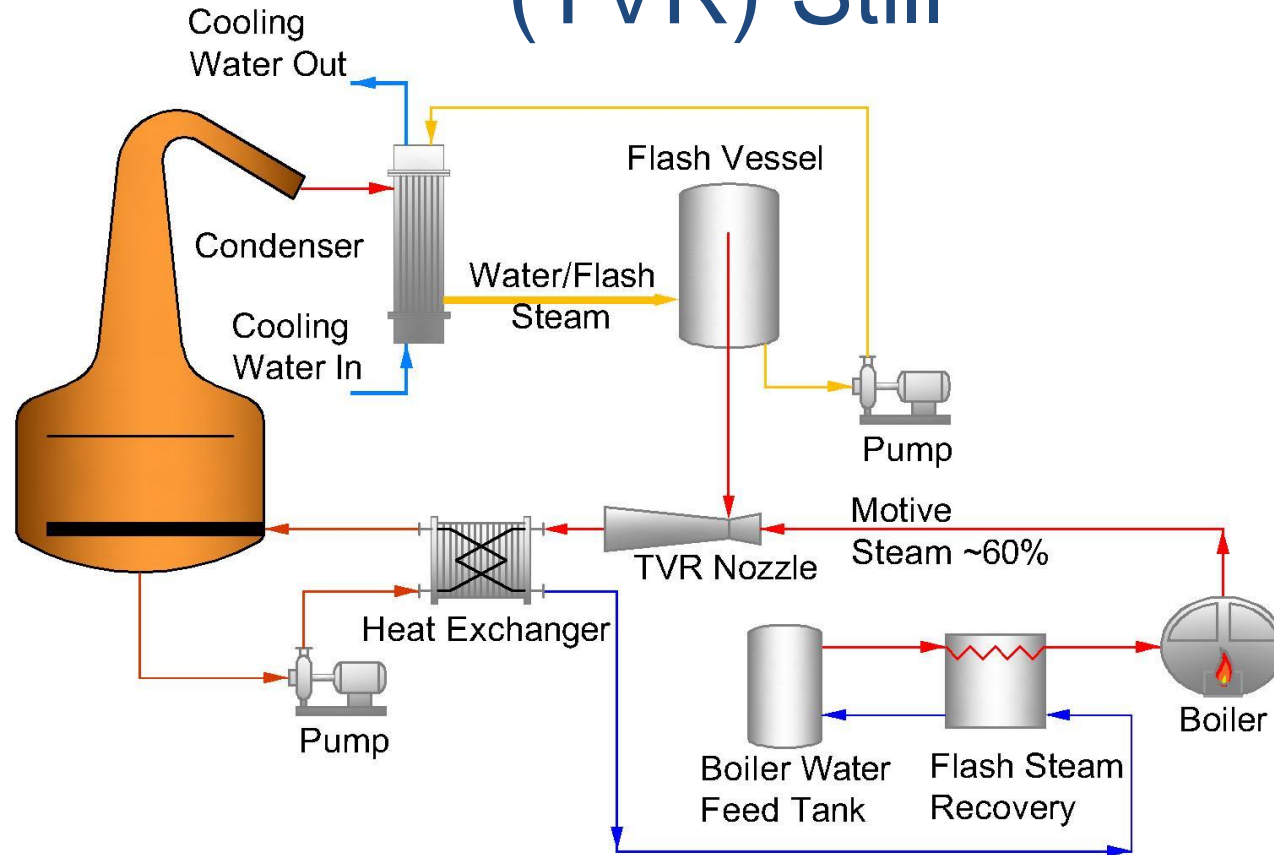
- Principle:
 - Density difference between Single Phase and Two Phase system
 - Creates Driving Force for the Thermosyphon recirculation



External Heater – Return above max level



Thermal Vapour Recompression (TVR) Still



TVR Features

Pros

- 40% Reduction in Batch Distillation Steam Usage for Scotch Whisky Wash Distillation ~ 5.5 kWh/ l alc
- Low Steam Pressure, coupled with good control and **pumped condensate systems** yield consistent batch times and low fouling levels

Cons

- Opex (Pump circulation)
- Generally complex operation (Automation & control)
- Condenser Life Reduced compared to traditional

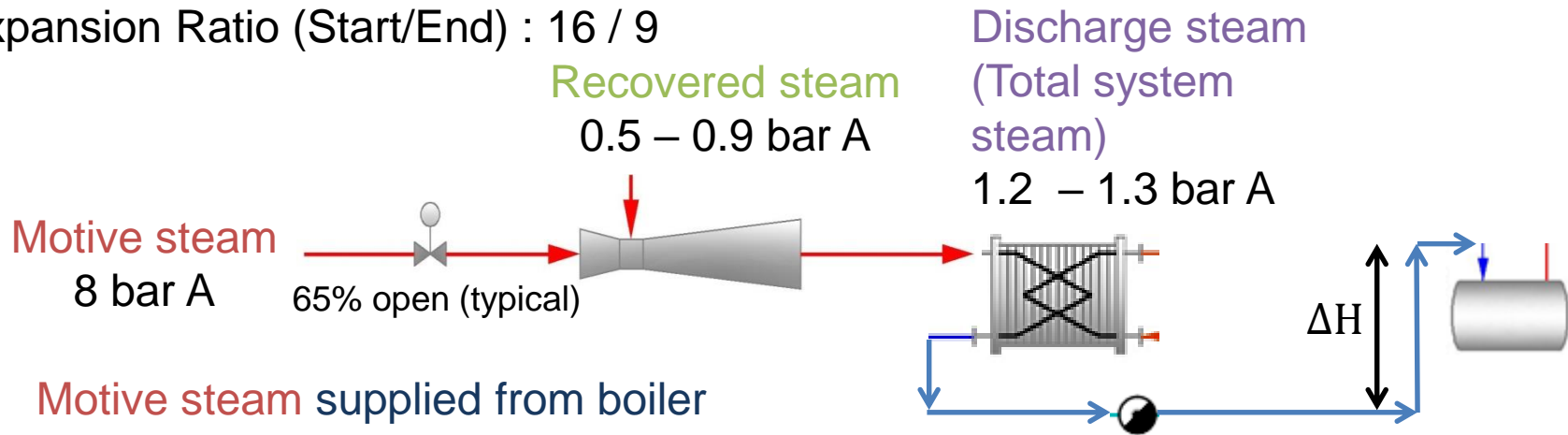


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TVR Steam Injector Nozzle

Compression Ratio (Start/End) : 2.4 / 1.4

Expansion Ratio (Start/End) : 16 / 9

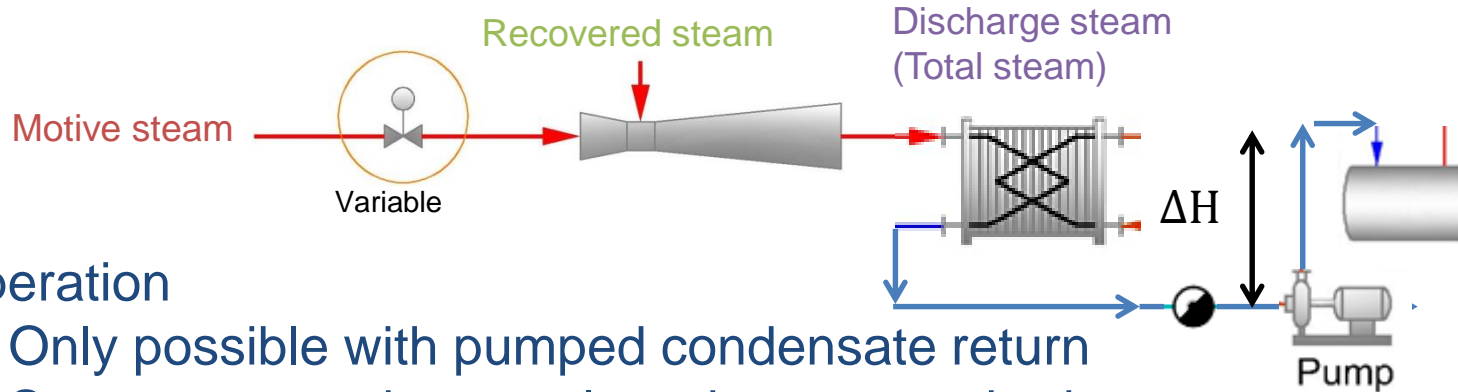


- **Motive steam** supplied from boiler
- A valve controls / throttles **motive steam** entering steam injector nozzle, steam required depends on compression ratio.
- **Motive steam** entrains the **recovered steam**
- **Discharge steam** heats the still and must be at sufficient pressure to push the condensate to drain/receiver

TVR Operation – Variable steam supply

Compression Ratio (Start/End) : 1.8 / 1.3

Expansion Ratio (Start/End) : 16 / 9



Operation

- Only possible with pumped condensate return
- Steam can condense at less than atmospheric pressure in the HX
- **Motive steam** is reduced as **recovered steam** increases

Distillation steam recovery

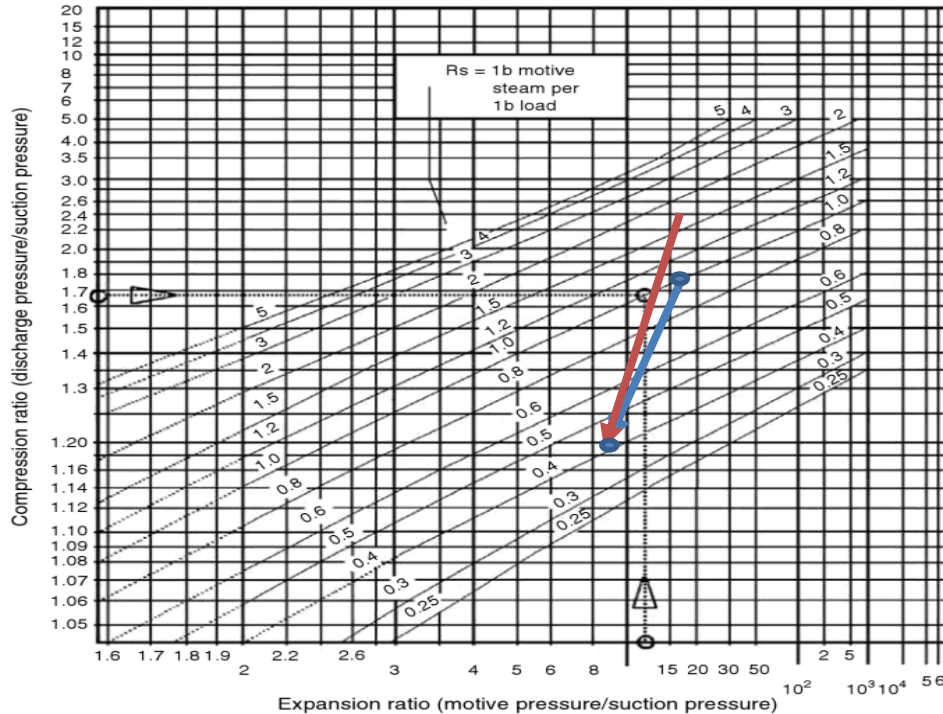
Theoretically:

Fixed motive steam

- 33 to 63 %
- Avg. = 48 %

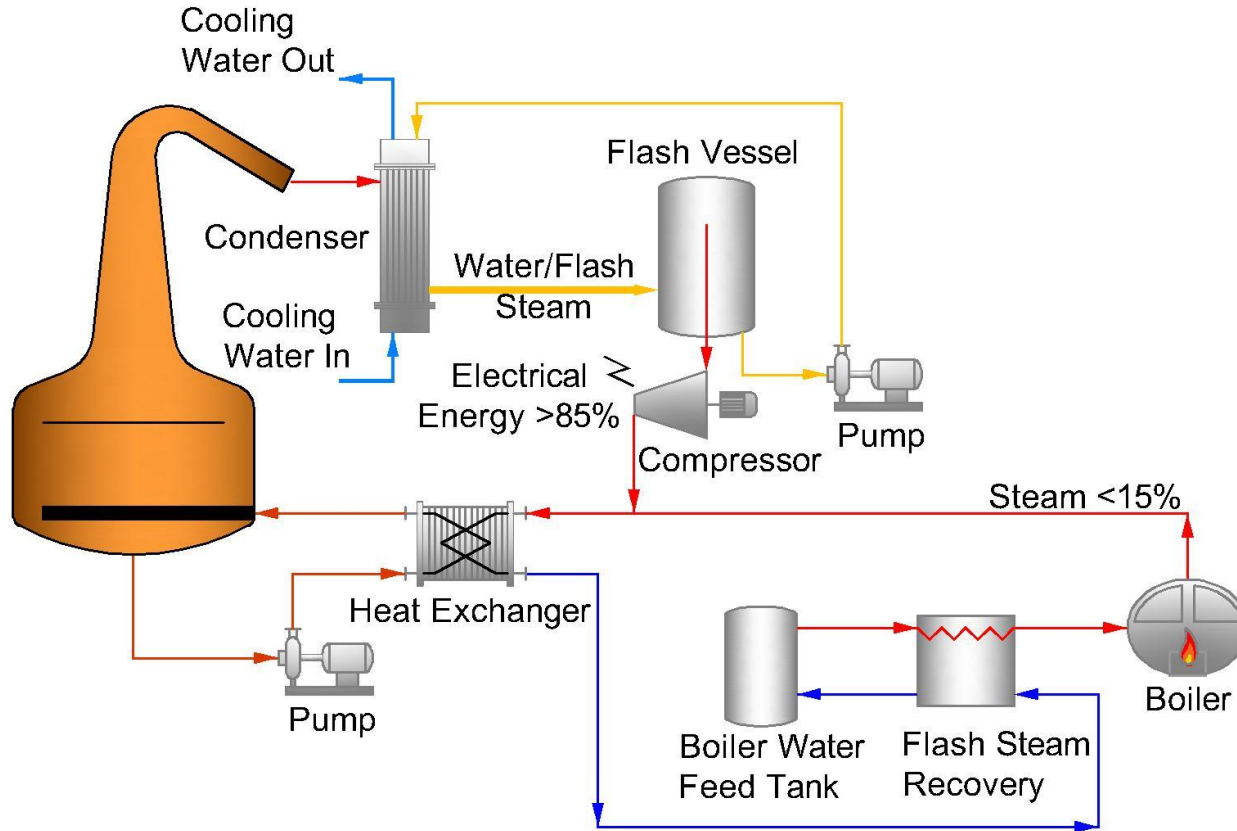
Variable motive steam

- 50 to 63 %
- Avg. = 56 %



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(HTHP) Still



HTHP Features

Pros

- >85% Reduction in Batch Distillation Steam Usage for Scotch Whisky Wash Distillation
 - 3.3 kWh / litre alc
- Low Steam Pressure, coupled with good control and **pumped condensate systems** yield consistent batch times and low fouling levels
- Reliance on Fossil Fuel Significantly reduced

Cons

- No examples in existence
 - Briggs Auchroisk-1985
- Generally complicated operation
 - Automation & control
- Condenser Life Reduced compared to traditional
- Payback Relative to Boiler Fuel and Electricity Price
- Opex (Pump circulation)



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Emulation of Direct Fired Character

- Bently Heritage Distillery, Minden, Nevada
 - build a modern, safe and efficient still house
 - recreate the rich, delicate character found from direct fired stills



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Distillery Wash

Character obtained from Still
Influenced by

- Raw Materials & Yeast
- Wort Separation Method
- Degree/length of Fermentation
- Heating Method & Reflux



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Maillard Reaction Temperatures

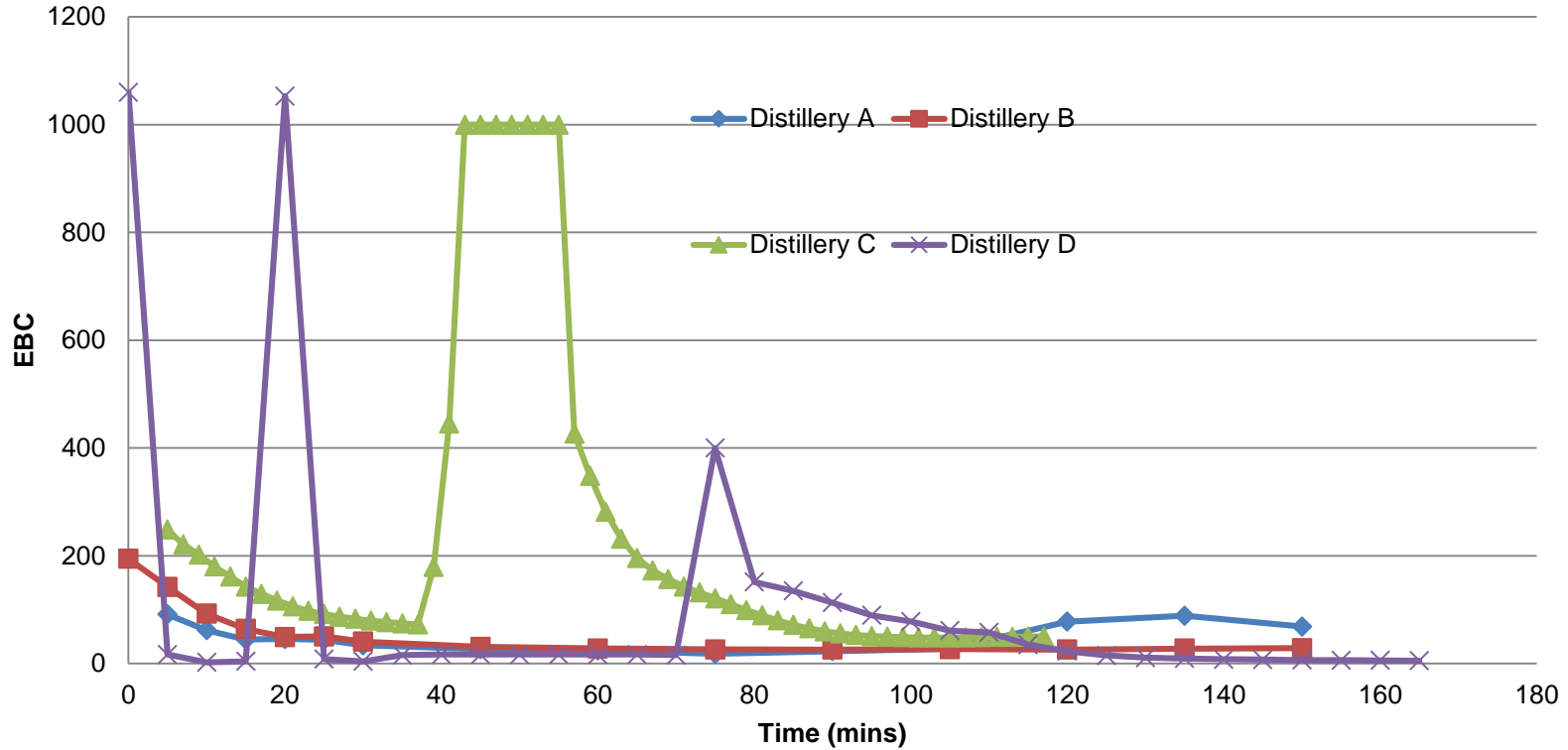
Flavour + colour =

- Water + (Temperature / Time) + (Amino acids + Sugar)

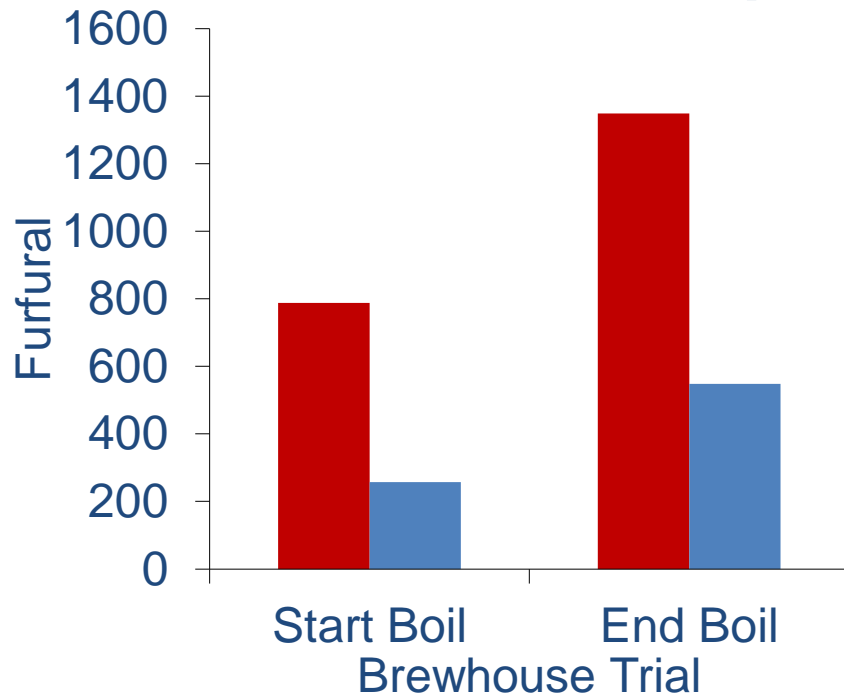
Still heating technology	TVR & HTHP	Steam	Thermal oil	Direct Fired
Operating temperature (°C)	107	135	185	>200



Wash Turbidity



Furfural level – Effect of Higher Temperatures



- 830 hl 6.5% / h x 70 min boil:
- **Internal Heater**
 - High Temperature Surface
 - $\sim 0.8 \text{ m}^2/\text{m}^3$
- High Surface Area Heater Low Temperature Surface
 - $2.2 \text{ m}^2/\text{m}^3$

External Thermal Oil Heater



- Thermal Oil Heating - 200°C, low pressure
- Control By Variable Area (Unlike Steam, Which is Variable Pressure/Temperature)

$$q = U \cdot A \cdot \Delta T$$

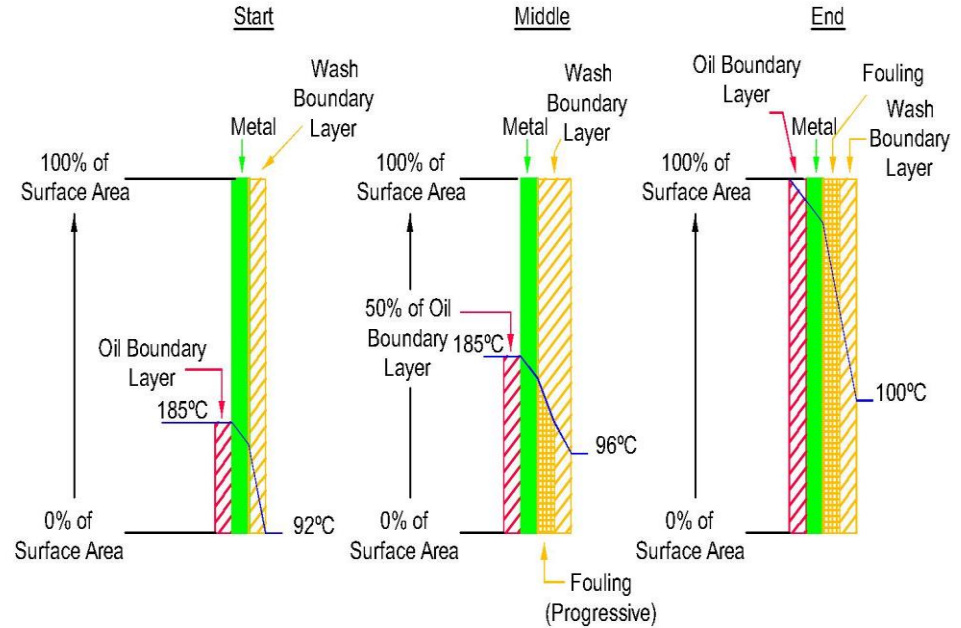
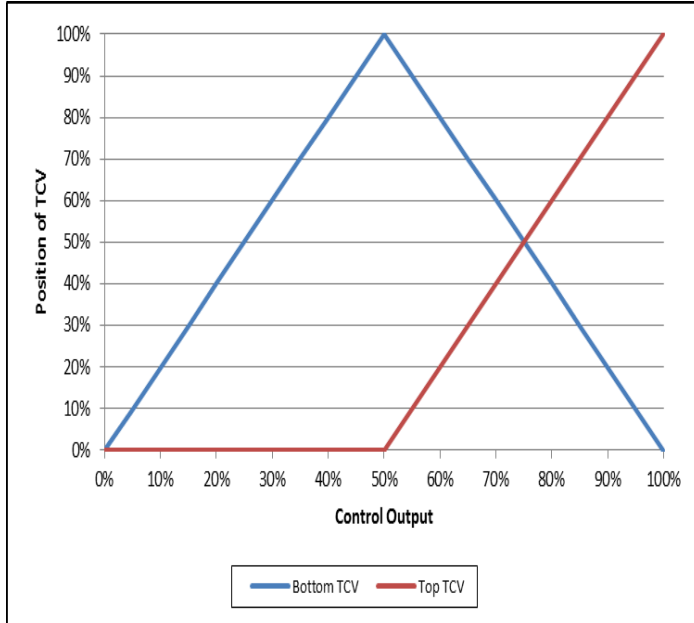
q = Heat Transfer (W) *[Rate of heat energy transfer per unit time]*

U = Overall Heat Transfer Coefficient (W/m².°C)

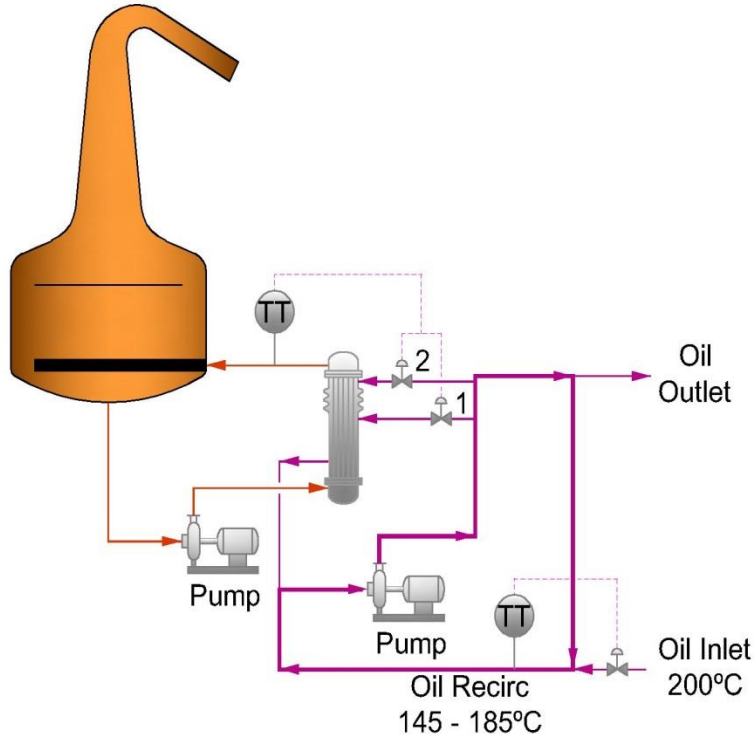
A = Heat Transfer Surface Area (m²)

ΔT = Temperature Difference (°C) *[Driving force]*

External Thermal Oil Heater



External Thermal Oil Heater



- Forced Circulation - reduce Fouling, no boil at heat transfer surface
- Oil Recirculation maintained at desired Temp (145 – 185 °C)
- Split Range Control of HX Surface Area, lower valve (1) opens first, if duty not achieved, valve (2) opens
- Progressive fouling of heat exchanger Area ie Area increased as Heat exchanger fouls.
- Film boil likely to limit max temp of thermal oil in practise



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Summary

- Method of Still heating is an important choice
- Flexible equipment can allow the distiller to select for specific characteristics



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Thanks For Your Time



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